

Prevalence of 'Candidatus Accumulibacter phosphatis' type II under phosphate limiting conditions

Welles, L.; Lopez-Vazquez, C. M.; Hooijmans, C. M.; van Loosdrecht, M. C M; Brdjanovic, D.

DOI

[10.1186/s13568-016-0214-z](https://doi.org/10.1186/s13568-016-0214-z)

Publication date

2016

Document Version

Final published version

Published in

AMB Express

Citation (APA)

Welles, L., Lopez-Vazquez, C. M., Hooijmans, C. M., van Loosdrecht, M. C. M., & Brdjanovic, D. (2016). Prevalence of 'Candidatus Accumulibacter phosphatis' type II under phosphate limiting conditions. *AMB Express*, 6, Article 44. <https://doi.org/10.1186/s13568-016-0214-z>

Important note

To cite this publication, please use the final published version (if applicable).
Please check the document version above.

Copyright

Other than for strictly personal use, it is not permitted to download, forward or distribute the text or part of it, without the consent of the author(s) and/or copyright holder(s), unless the work is under an open content license such as Creative Commons.

Takedown policy

Please contact us and provide details if you believe this document breaches copyrights.
We will remove access to the work immediately and investigate your claim.

ORIGINAL ARTICLE

Open Access



Prevalence of '*Candidatus* Accumulibacter phosphatis' type II under phosphate limiting conditions

L. Welles^{1,2*}, C. M. Lopez-Vazquez¹, C. M. Hooijmans¹, M. C. M. van Loosdrecht^{2,3} and D. Brdjanovic^{1,2}

Abstract

P-limitation in enhanced biological phosphorus removal (EBPR) systems fed with acetate, has generally been considered as a condition leading to enrichment of organisms of the genotype '*Candidatus* Competibacter phosphatis' expressing the glycogen-accumulating organisms (GAO) phenotype. Recent studies have demonstrated in short-term experiments that organisms of the genotype '*Candidatus* Accumulibacter phosphatis' clade I and II, known to express the polyphosphate-accumulating organisms (PAO) phenotype can switch to the GAO phenotype when poly-P is absent, but are performing the HAC-uptake at lower kinetic rates, where clade I showed the lowest rates. The objective of this study was to verify whether organisms of the genotype '*Candidatus* Accumulibacter phosphatis' can also be enriched under P-limiting conditions while expressing a GAO phenotype and more specifically to see which specific clade prevails. A sequencing batch reactor was inoculated with activated sludge to enrich an EBPR culture for a cultivation period of 128 days (16 times the solids retention time) under P-limiting conditions. A mixed culture was obtained comprising of 49 % '*Candidatus* Accumulibacter phosphatis' clade II and 46 % '*Candidatus* Competibacter phosphatis'. The culture performed a full GAO metabolism for anaerobic HAC-uptake, but was still able to switch to a PAO metabolism, taking up excessive amounts of phosphate during the aerobic phase when it became available in the influent. These findings show that P-limitation, often used as strategy for enrichment of '*Candidatus* Competibacter phosphatis', does not always lead to enrichment of only '*Candidatus* Competibacter phosphatis'. Furthermore, it demonstrates that '*Candidatus* Accumulibacter phosphatis' are able to proliferate in activated sludge systems for periods of up to 128 days or longer when the influent phosphate concentrations are just enough for assimilation purposes and no poly-P is formed. The '*Candidatus* Accumulibacter phosphatis' retain the ability to switch to the PAO phenotype, taking up phosphate from the influent as soon as it becomes available.

Keywords: Polyphosphate-accumulating organisms (PAO), Glycogen-accumulating organisms (GAO), Enhanced biological phosphate removal (EBPR), Polyphosphate content, Microbial ecology, Niche differentiation, '*Candidatus* Accumulibacter phosphatis', '*Candidatus* Competibacter phosphatis'

Introduction

Enhanced biological phosphorus removal (EBPR) is a microbial process for removal of excessive amounts of phosphorus from wastewater through storage of intracellular polyphosphate (poly-P) by polyphosphate-accumulating organisms (PAO) and excess sludge wasting.

Due to its high efficiency and cost-effectiveness, the process is widely implemented in biological wastewater treatment systems. When activated sludge is cycled through alternating anaerobic and aerobic zones, organisms with the PAO phenotype are able to take up phosphate from the liquid phase and store it as intracellular polyphosphate, leading to P-removal from the bulk liquid via PAO cell removal through the wastage of activated sludge. These organisms take up volatile fatty acids (VFA) under anaerobic conditions and store it as poly- β -hydroxyalkanoates (PHA) (Wentzel et al. 1985; Comeau

*Correspondence: laurens.welles@gmail.com

¹ Department of Environmental Engineering and Water Technology, UNESCO-IHE Institute for Water Education, Westvest 7, 2611AX Delft, The Netherlands

Full list of author information is available at the end of the article

et al. 1986; Mino et al. 1987). The uptake and storage of VFA requires energy, which can be generated by poly-P cleavage and subsequent release of ortho-phosphate. In the following aerobic phase, the organisms oxidize PHA and use the energy to restore their poly-P pool along with other metabolic processes. By linking microbial community composition with EBPR performance, “*Candidatus Accumulibacter phosphatis*” were identified as the organisms expressing the PAO phenotype in many laboratory EBPR systems (Bond et al. 1995, 1999; Hesselman et al. 1999; Crocetti et al. 2000) as well as full-scale waste water treatment plants (Zilles et al. 2002; Kong et al. 2004; Gu et al. 2005; He et al. 2005; Wong et al. 2005). Another group of organisms, ‘*Candidatus Competibacter phosphatis*’, are considered to compete with ‘*Candidatus Accumulibacter phosphatis*’ for acetate (HAc), expressing a so called glycogen-accumulating organisms (GAO) phenotype (Mino et al. 1987; Nielsen et al. 1999; Crocetti et al. 2002). The only difference is that for the GAO phenotype, glycogen is used as energy source instead of poly-P, for the uptake and storage of HAc and therefore they do not contribute to EBPR. Prevalence of ‘*Candidatus Competibacter phosphatis*’ is considered to be an important factor that leads to EBPR deterioration. Hence, the competition between ‘*Candidatus Accumulibacter phosphatis*’ and ‘*Candidatus Competibacter phosphatis*’ communities in EBPR processes has been the subject of several laboratory studies, often using highly enriched EBPR cultures expressing the PAO and GAO phenotypes (Oehmen et al. 2007).

To study factors affecting the competition between organisms that express the PAO and GAO phenotypes, it is necessary to obtain highly enriched ‘*Candidatus Accumulibacter phosphatis*’ and ‘*Candidatus Competibacter phosphatis*’ cultures. Influent phosphorus limitation has often been used as a strategy to enrich ‘*Candidatus Competibacter phosphatis*’ (Sudiana et al. 1999; Filipe et al. 2001; Zeng et al. 2003; Lopez-Vazquez et al. 2007). Mostly, since it was considered that ‘*Candidatus Accumulibacter phosphatis*’ were dependent on poly-P and would wash-out of the system once the phosphate concentrations became limiting. However, recent studies have shown in short-term experiments that ‘*Candidatus Accumulibacter phosphatis*’ are capable of performing a GAO metabolism (i.e. using glycogen to produce all of the required energy for VFA uptake) (Zhou et al. 2008; Acevedo et al. 2012) at lower kinetic rates. These new insights led to the speculation that P-limitation may not always lead to highly enriched ‘*Candidatus Competibacter phosphatis*’ cultures. This would also imply that biomass cultures enriched in previous studies, that seemed to be ‘*Candidatus Competibacter phosphatis*’ cultures, may have actually been ‘*Candidatus Accumulibacter*

phosphatis’ cultures that performed a GAO metabolism, if no microbial characterization methods were applied that could distinguish ‘*Candidatus Accumulibacter phosphatis*’ and ‘*Candidatus Competibacter phosphatis*’ populations (as in Liu et al. 1997; Sudiana et al. 1999; Schuler and Jenkins 2003). Therefore, it is important to (re-)investigate which microbial populations will develop in EBPR systems operated under phosphate limiting conditions.

Besides the selection of ‘*Candidatus Accumulibacter phosphatis*’ and ‘*Candidatus Competibacter phosphatis*’, it is also important to verify which ‘*Candidatus Accumulibacter phosphatis*’ clades may proliferate under phosphate limiting conditions, as this may help to develop an enrichment strategy specifically for ‘*Candidatus Accumulibacter phosphatis*’ clade I or II. The intrinsic differences within the metabolic characteristics of the ‘*Candidatus Accumulibacter phosphatis*’ clades (Carvalho et al. 2007; Flowers et al. 2009; Slater et al. 2010), urges the need to study these metabolic differences and develop clade specific metabolic models for better understanding and description of EBPR processes. For this purpose, it is necessary to develop strategies for the selection of specific ‘*Candidatus Accumulibacter phosphatis*’ clades to obtain EBPR cultures highly enriched with specific clades.

A recent study suggested that ‘*Candidatus Accumulibacter phosphatis*’ clade II may have a competitive advantage over ‘*Candidatus Accumulibacter phosphatis*’ clade I under short-term poly-P depleted conditions (Acevedo et al. 2012). Moreover, through short-term batch tests it was shown that the HAc-uptake rate of ‘*Candidatus Accumulibacter phosphatis*’ clade II was four times faster than that of ‘*Candidatus Accumulibacter phosphatis*’ clade I under poly-P depleted conditions (Welles et al. 2015). Therefore, low influent P/C ratios or the periodical phosphate limitation may lead to ‘*Candidatus Accumulibacter phosphatis*’ clade II enrichments while high P/C influent ratios may support the development of ‘*Candidatus Accumulibacter phosphatis*’ clade I cultures.

The objectives of this study were: (i) to reinvestigate which bacterial populations can develop in EBPR systems inoculated with activated sludge operated for a long-term period under phosphate limiting conditions, (ii) to assess whether ‘*Candidatus Accumulibacter phosphatis*’ can get enriched and, if so, which specific clade would prevail, and (iii) to verify whether ‘*Candidatus Accumulibacter phosphatis*’ enriched under phosphate limiting conditions are capable of taking up excessive amounts of phosphate when they are suddenly exposed to high phosphate concentrations. This study contributes to the fundamental understanding of the ‘*Candidatus Accumulibacter phosphatis*’ metabolism and clade differentiation, helps to improve the strategies for ‘*Candidatus Competibacter*

phosphatis' and/or '*Candidatus Accumulibacter phosphatis*' clade II enrichment and provides insight into the EBPR performance of WWTPs that may (periodically) suffer from phosphate limiting conditions.

Materials and methods

Bacterial enrichment under phosphate limiting conditions

Operation of sequencing batch reactors

An EBPR culture was enriched in a double-jacketed laboratory sequencing batch reactors (SBR) under the same conditions as those previously described for GAO by Welles et al. (2014). The SBR had a working volume of 2.5 l. Activated sludge from a municipal wastewater treatment plant (Hoek van Holland, The Netherlands) was used as inoculum. The SBR was operated in cycles of 6 h (2.25 h anaerobic, 2.25 h aerobic and 1.5 h settling phase) following similar operating conditions used in previous studies (Smolders et al. 1994). The SBR was operated at a pH value of 7.0 ± 0.05 and a temperature of 20 ± 1 °C. The applied solids retention time (SRT) was 8 days.

Synthetic medium

The SBR was fed with synthetic medium. The influent phosphate concentration was $0.071 \text{ P-mmol l}^{-1}$ (2.2 mg $\text{PO}_4\text{-P l}^{-1}$) (Liu et al. 1997) and the acetate concentration was $12.6 \text{ C-mmol l}^{-1}$ (373 mg HAc l^{-1} , 400 mg COD l^{-1} , 860 mg $\text{NaAc}\cdot 3\text{H}_2\text{O}$), leading to an influent P/C ratio of 0.0056 (P-mol C-mol $^{-1}$). Further details regarding other macronutrients and trace elements can be found in Smolders et al. (1994).

Monitoring of SBR

The performance of the SBR was regularly monitored by measuring the total suspended solids (TSS), volatile suspended solids (VSS) and inorganic suspended solids (ISS). The (pseudo) steady-state conditions in the reactor was confirmed by daily determination of the aforementioned parameters as well as online pH and dissolved oxygen (DO) profiles. When no significant changes of these parameters and the characteristic online DO and pH profiles were observed for a time interval of three SRT, the enrichment culture was considered to be in pseudo steady-state.

Characterization of the microbial community

An estimation of the degree of enrichment of the bacterial populations of interest ('*Candidatus Accumulibacter phosphatis*' clade I, clade II and '*Candidatus Competibacter phosphatis*') was undertaken via fluorescence in situ hybridization (FISH) microscopy analyses. Biomass samples were fixed in 4 % paraformaldehyde and incubated for 120 min at room temperature. After fixation, samples were centrifuged for 2 min at 6000 rpm,

washed twice in $1\times$ Phosphate buffer saline (PBS), re-suspended in an ethanol/PBS buffer mixture (volume 1:1) and finally stored at -20 °C. For hybridization, the fixed samples were dried on gelatin coated wells of hybridization slides. The samples were dehydrated by passing the microscope slides through 50, 80 and 100 % ethanol solutions for 3 min in each solution. After dehydration, the hybridization solution (10 μl) and 1 μl of oligonucleotide probe (tagged with the fluorescent labels Fluos, Cy5 or Cy3) solution (with concentration of 8.3, 5 and 5 pmol/L for Fluos, CY5 and CY3 labels, respectively) was added to each well, and the samples were immediately incubated for 2 h in a humid chamber at 46 °C. The hybridization buffer consisted of a mixture of 360 μl of 5 M NaCl, 40 μl of 1 M Tris (pH 8), 10 μl of a 10 % (w/v) sodium dodecylsulfate buffer (SDS), 700 μl of formamide, and 900 μl of MilliQ water (Amann et al. 1990; Crocetti et al. 2000, 2002; Daims et al. 1999). After hybridization, the microscope slides were washed at 48 °C for 12 min by immersing them into 50 ml of washing solution. The washing solution consisted of 800 μl of 5 M NaCl, 500 μl of 0.5 M EDTA, 1000 μl of 1 M Tris (pH8), and 50 μl of 10 % SDS(w/v). The samples were dried and prepared with 2 ml antifade fluorescent mounting oil. The probes used to target the organisms of interest are shown in Table 1. The whole bacterial community was targeted by the EUB-338mix (mix of general bacteria probes EUB, EUB II and EUB III). '*Candidatus Accumulibacter phosphatis*' was targeted by the PAO651 probe whereas GAOMIX probe (mixture of probes GAOQ431 and GAOQ989) was used to target '*Candidatus Competibacter phosphatis*'. '*Candidatus Accumulibacter phosphatis*' clade I (clade IA and other type I clades) and '*Candidatus Accumulibacter phosphatis*' clade II (clade IIA, IIC and IID) were targeted by the probes Acc-1-444 and Acc-2-444, respectively. Hybridized samples were examined with Zeiss Axio-plan-2 epifluorescence microscope. The quantification of the '*Candidatus Accumulibacter phosphatis*' and '*Candidatus Competibacter phosphatis*' biomass fractions (of the entire bacterial community) and the '*Candidatus Accumulibacter phosphatis*' clade I and II fractions (of the '*Candidatus Accumulibacter phosphatis*' community) in the biomass was carried out via FISH image analysis using the free ImageJ software package (version 1.47b, Wayne Rasband, National Institute of Health, USA). For each quantification 18 randomly selected FISH images were analysed. For the PAO and GAO fractions, the surface area of cells binding the specific PAO651 and GAOmix probes were expressed as the mean percentage of the surface area of cells binding the entire bacterial community (EUBmix). For the PAO I and PAO II fraction, the surface area of cells binding the specific PAOmix and GAOmix probes were expressed as the mean percentage

Table 1 Overview of probes used to target the organisms of interest for the FISH microscopic analysis of the enrichment culture

Reference	Probe	Sequence (5'–3')	Target	Formamide (%)
Amann et al. (1990)	EUB	GCTGCTCCCGTAGGAGT	Many but not all Bacteria	0–70
Daims et al. (1999)	EUB II	GCAGCCACCCGTAGGTGT	Planctomycetales	0–50
Daims et al. (1999)	EUB III	GCTGCCACCCGTAGGTGT	Verrucomicrobiales	0–50
Crocetti et al. (2000)	PAO 651	CCCTCTGCCAACTCCAG	'Candidatus Accumulibacter phosphatis'	35
Crocetti et al. (2002)	GAOQ431	TCCCCGCCTAAAGGGCTT	'Candidatus Competibacter phosphatis'	35
Crocetti et al. (2002)	GAOQ989	TTCCCCGGATGTCAAGGC	'Candidatus Competibacter phosphatis'	35
Flowers et al. (2009)	Acc-I-444	CCCAAGCAATTCTTCCCC	'Candidatus Accumulibacter phosphatis' Clade IA and other Type I clades	35
Flowers et al. (2009)	Acc-II-444	CCC GTGCAATTCTTCCCC	'Candidatus Accumulibacter phosphatis' Clade IIA, IIC and IID	35

of the surface area of cells binding the entire PAO community (PAOmix). The standard error of the mean (SEM) was calculated as the standard deviation of the area percentage divided by the square root of the number of images for each quantification.

Characterization of anaerobic carbon and phosphate conversions

When the SBR reached pseudo steady-state conditions, a cycle was intensively monitored to determine the biomass kinetic rates and stoichiometry of the anaerobic conversions. In addition to the above described parameters, orthophosphate ($\text{PO}_4^{3-}\text{-P}$), acetate (HAc-C), PHA and glycogen were measured in the cycle. To verify if the enriched culture was able to take up excessive amounts of phosphate, two consecutive cycles were conducted in which a concentrated phosphate solution was added at the end of the anaerobic phase prior to the aerobic stage. This phosphate addition led to an increase of 0.65 P-mmol l^{-1} in the reactor. In the following aerobic phase, the phosphate concentration was intensively monitored.

Analyses

The determinations of TSS, VSS and ISS were performed in triplicates in accordance with Standard Methods (A.P.H.A. 1995). For the TSS analysis, well-mixed samples with a volume of 10 mL were filtered through weighed standard glass-fiber filters (Whatman GF/C, diameter 47 mm). After filtration of the samples, an additional 10 ml of tap water was filtered to wash away dissolved solids in the remaining liquid phase in the filters and residues. The residues retained on the filters were dried for 24 h at 103–105 °C. The increase in weight of the filters represented the total suspended solids (TSS) concentration. The residues were ignited for 3 h at 520 °C. The remaining solids represented the fixed suspended solids (ISS) concentrations, while the weight lost on ignition represented the volatile suspended solids (VSS) concentrations. $\text{PO}_4\text{-P}$ was determined by the

ascorbic acid method in accordance with Standard Methods (A.P.H.A. 1995). HAc was determined using a Varian 430-GC Gas Chromatograph (GC), equipped with a split injector (split ratio 1:10), a WCOT Fused Silica column with a FFAP-CB coating (25 m $\times$ 0.53 mm $\times$ 1 μm), and coupled to a FID detector. Helium gas was used as carrier gas. The temperature of the injector, column and detector was 200, 105 and 300 °C, respectively. Glycogen was determined according to the method described by Smolders et al. (1994) but with an extended digestion of 5 h in 5 ml 0.9 mol l^{-1} HCl, using 5 mg of freeze dried biomass as described by Lanham et al. (2012). The poly- β -hydroxybutyrate PHB and poly- β -hydroxyvalerate (PHV) contents of freeze dried biomass were determined according to the method described by Smolders et al. (1994). The non-soluble total phosphorus concentration (Pns) at the end of the aerobic (and beginning of the cycle was determined on the basis of the steady state mass balance for phosphorus using Eqs. 1a–d. Pns at the end of the anaerobic phase was determined by subtracting the ortho-phosphate concentration at the end of the anaerobic phase from the steady state aerobic Pns.

$$\begin{aligned} d(T_{P,e} * V_p)/dt \\ = Q_i * (T_{P,i} - T_{P,e}) - Q_w * \text{TSS} * f_{P,\text{TSS}} = 0 \end{aligned} \quad (1a)$$

$$Q_i/V_p * (T_{P,i} - T_{P,e}) - Q_w/V_p * \text{TSS} * f_{P,\text{TSS}} = 0 \quad (1b)$$

$$1/\text{HRT} * (T_{P,i} - T_{P,e}) - 1/\text{SRT} * \text{TSS} * f_{P,\text{TSS}} = 0 \quad (1c)$$

$$\text{Pns} = \text{SRT}/\text{HRT} * (T_{P,i} - T_{P,e}) \quad (1d)$$

where TSS: concentration of total suspended solids, Pns: concentration of non-soluble total phosphorus, $T_{P,i}$: total phosphorus concentration in the influent, $T_{P,e}$: total phosphorus concentration in the effluent, $f_{P,\text{TSS}}$: ratio of

total P per TSS, V_p : working volume of reactor, Q_i : influent flow rate, Q_w : wastage of activated sludge flow rate, HRT: hydraulic retention time and SRT: solids retention time.

Determination of kinetic and stoichiometric parameters

The kinetic rate of interest was the anaerobic HAC-uptake rate. This rate was expressed as maximum active biomass specific rate based on the HAC profiles observed in the tests as described by Smolders et al. (1994) and Brdjanovic et al. (1997). The stoichiometric ratios of interest were P/HAC, PHV/PHB, PHV/HAC, PHB/HAC and gly/HAC.

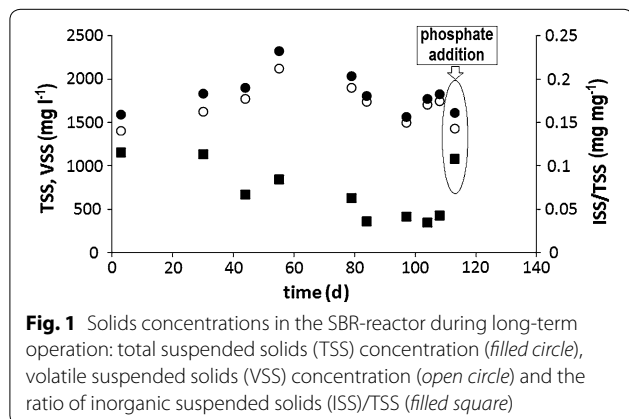
Results

Enrichment of EBPR culture under phosphate limiting conditions

After inoculation, the online pH and DO profiles indicated that within approximately 10 SRT (80 days) the performance of the reactor reached steady-state conditions. In Fig. 1, the TSS and VSS concentrations as well as the ISS/TSS ratio are shown. Although the TSS and VSS concentrations fluctuated during the period of enrichment, the average TSS and VSS concentrations (1.9 gTSS l^{-1} , 1.8 gVSS l^{-1}) of this period were in the range of concentrations observed in similar previous studies. The ISS/TSS ratio of the inoculum was 0.12 mg mg^{-1} . This gradually decreased to a value of 0.04 mg mg^{-1} , except for the last data point which was obtained after conducting a batch experiment with an additional phosphate feed. The low ISS/TSS ratio observed in this study under steady-state conditions (0.04 mg mg^{-1}), in comparison to typical ISS/TSS ratios of high grade PAO enrichments [0.60 mg mg^{-1} (Schuler and Jenkins 2003a)] indicates that the sludge did not contain significant quantities of poly-P as expected from the experimental design with the low influent phosphate concentration. On the basis of the steady state mass balance (and the low influent

phosphate concentration), the Pns (non-soluble total phosphorus concentration) in the system was determined as $1.1 \text{ P-mmol l}^{-1}$ (35 mgP/l) (Eq. 1d) and the Pns/VSS ratio was determined as $0.019 \text{ mgP mgVSS}^{-1}$. These values are in the range of normal non-EBPR biomass ($0.023 \text{ Metcalf and Eddy 2003}$) and demonstrate that there is practically no poly-P present in the sludge. As '*Candidatus Accumulibacter phosphatis*' are considered to rely on intracellular poly-P for anaerobic substrate uptake, it was expected that they were no longer present in this sludge.

After approximately 14 SRT (113 days), the composition of the microbial community was analyzed. In Fig. 2, FISH images and phase contrast images of the enriched culture are shown. Figure 2a remarkably shows that both '*Candidatus Accumulibacter phosphatis*' and '*Candidatus Competibacter phosphatis*' were present in similar quantities. Additional FISH analyses showed that among the '*Candidatus Accumulibacter phosphatis*' clades, clade II was dominant whereas the presence of clade I was negligible. FISH quantification showed that the '*Candidatus Accumulibacter phosphatis*' and '*Candidatus Competibacter phosphatis*' fractions of the total bacterial population were 49 ± 6 and 46 ± 7 %, respectively (see Additional file 1 for raw FISH images). Based on these '*Candidatus Accumulibacter phosphatis*' and '*Candidatus Competibacter phosphatis*' fractions, the '*Candidatus Accumulibacter phosphatis*'/'*Candidatus Competibacter phosphatis*' ratio was around 1:1. The '*Candidatus Accumulibacter phosphatis*' clade I and II fractions with regard to the '*Candidatus Accumulibacter phosphatis*' population were 0 ± 0 % ($n = 16$) and 99 ± 2 % ($n = 16$), respectively. In Fig. 2c and d, phase contrast images of the biomass are presented, showing the prevalence (Fig. 2c) of two groups of organisms with distinct morphotypes (coccus and rod) (Fig. 2d). By comparing the phase contrast and the FISH images (Additional file 1), the organisms with the rod morphology were identified as '*Candidatus Accumulibacter phosphatis*' and those with the coccus morphology as '*Candidatus Competibacter phosphatis*'.



Biochemical conversions

To confirm the absence of a poly-P dependent metabolism for anaerobic substrate uptake under steady-state conditions, the carbon and phosphate conversions were monitored during one cycle after approximately 11 SRT (84 days) (Fig. 3a). During the anaerobic phase, all HAC ($6.25 \text{ C-mmol l}^{-1}$) was taken up in less than 1 h with an active biomass specific HAC-uptake rate of $144 \text{ (C-mmol (C-mol h)}^{-1})$ and this HAC-uptake was coupled to a net P-release of $0.09 \text{ P-mmol l}^{-1}$ (2.7 mgP l^{-1}). This led to a P-release/HAC-uptake ratio of $0.01 \text{ P-mol C-mol}^{-1}$, which indicates a negligible involvement of poly-P in

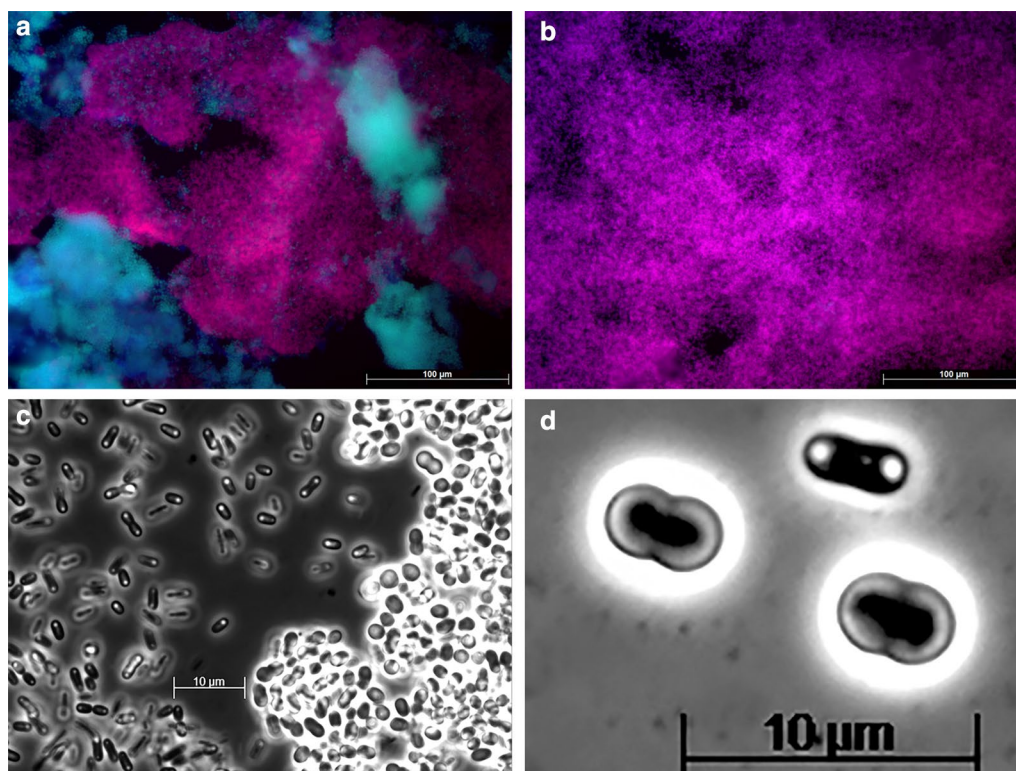


Fig. 2 Representative FISH-microscopy images (**a, b**) and phase contrast images (**c, d**) showing the distribution of bacterial populations in the enriched biomass culture. In **a**, blue (EUB mix, Cy5): all bacteria other than '*Candidatus Accumulibacter phosphatis*' and '*Candidatus Competibacter phosphatis*'; purple (superposition of PAO mix 651, Cy3 and EUB mix, Cy5): '*Candidatus Accumulibacter phosphatis*'; and cyan green (superposition of GAO mix, Fluos and EUB mix, Cy5): '*Candidatus Competibacter phosphatis*'. In **b**, blue (PAO mix 651, Cy5): all potential PAO that do not stain with specific probes for '*Candidatus Accumulibacter phosphatis*' type I and II, purple (superposition of PAO mix 651, Cy5 and Acc II, Cy3): '*Candidatus Accumulibacter phosphatis*' type II, and cyan green (superposition of PAO mix 651, Cy5 and Acc I, Fluos): '*Candidatus Accumulibacter phosphatis*' type I. In **c**, dark cells: bacteria with the typical '*Candidatus Accumulibacter phosphatis*' morphology; bright cells: bacteria with the typical '*Candidatus Competibacter phosphatis*' morphology. In **d**, small size: bacteria with the typical '*Candidatus Accumulibacter phosphatis*' morphology; big size: bacteria with the typical '*Candidatus Competibacter phosphatis*' morphology

the anaerobic conversions when compared to typical ratios [P-release/HAc-uptake ratios as high as 0.75 P-mol C-mol⁻¹ (Schuler and Jenkins 2003)] of high grade PAO enrichment cultures. The stoichiometric values of the anaerobic carbon and phosphate conversions are given in Table 2. The high gly/HAc ratio, high PHV/PHB as well as the other stoichiometric values are characteristic for a fully glycogen dependent metabolism as observed in enriched GAO cultures, in which the energy production from poly-P degradation in the PAO metabolism is substituted by energy production through glycogen conversion into PHA.

To verify if the '*Candidatus Accumulibacter phosphatis*', that seemed to be present, were able to take up phosphate, two consecutive cycle tests were conducted after approximately 14 SRT (113 days), in which 0.65 P-mmol l⁻¹ (20 mgP l⁻¹) was added to the reactor at the end of each anaerobic phase (Fig. 3b). In the first cycle, 0.6 P-mmol l⁻¹ (18 mgP l⁻¹) was taken up while in

the second cycle 0.7 P-mmol l⁻¹ (21 mgP l⁻¹) was taken up (data not shown) in total 1.26 P-mmol l⁻¹ (39 mgP l⁻¹) in two consecutive cycles, which is about 17 times more phosphorus removal in comparison to the phosphorus removal observed during the normal operation of the system. Considering that for the assimilation of biomass in the two consecutive cycles only 0.07 P-mmol l⁻¹ (2.1 mgP l⁻¹) was needed and that chemical precipitation at pH 7.0 with low calcium concentrations is not likely to occur, this ortho-phosphate removal confirms that the '*Candidatus Accumulibacter phosphatis*' observed by microscopy were present, and that they were able to remove excessive amounts of phosphate from the liquid phase. This was further confirmed by the increase in the ISS/TSS ratio. The storage of 1.26 P-mmol l⁻¹ (39 mgP l⁻¹) as poly-P is equivalent to 0.13 gISS l⁻¹, assuming a poly-P composition of (KMg(PO₃)₃). With a TSS concentration of 1.6 gTSS l⁻¹, this increase in the ISS concentration would make a difference of 0.08 mg mg⁻¹

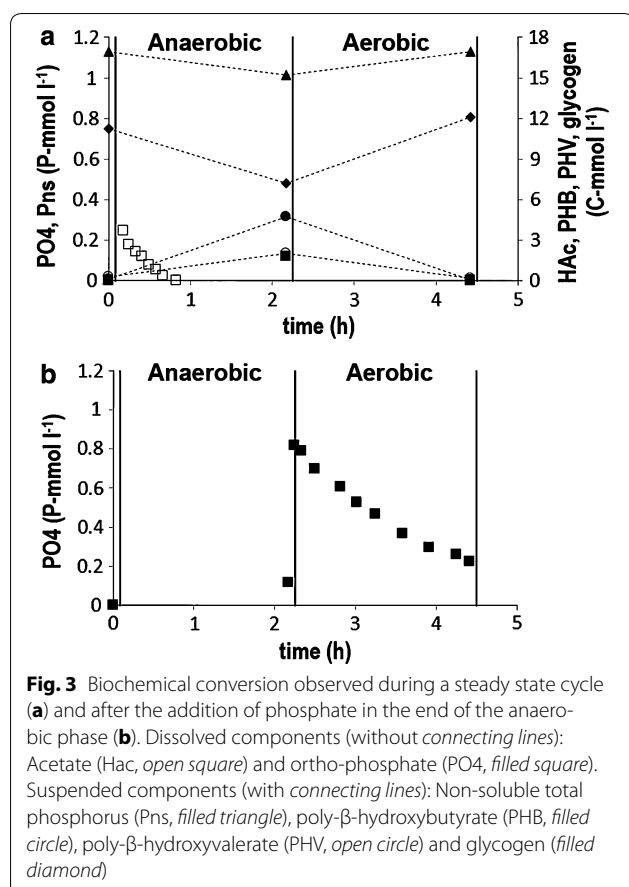


Fig. 3 Biochemical conversion observed during a steady state cycle (a) and after the addition of phosphate in the end of the anaerobic phase (b). Dissolved components (without connecting lines): Acetate (HAc, open square) and ortho-phosphate (PO₄, filled square). Suspended components (with connecting lines): Non-soluble total phosphorus (P_{ns}, filled triangle), poly-β-hydroxybutyrate (PHB, filled circle), poly-β-hydroxyvalerate (PHV, open circle) and glycogen (filled diamond)

in the ISS/TSS ratio, which approximately corresponds to the increase in the ISS/TSS ratio shown in Fig. 1.

Discussion

Enrichment of mixed cultures of '*Candidatus Accumulibacter phosphatis*' and '*Candidatus Competibacter phosphatis*'

Bacterial populations cultivated in continuous and sequencing batch reactors will always wash-out (i) from continuously operated reactors if the maximum growth rate of the organisms is lower than the dilution rate or (ii) in SBR reactors if the maximum net growth per cycle is lower than the net biomass removal per cycle. If, bacteria are not able to grow at all, then in the ideal case it would take only 1 SRT to wash-out more than 64 % of the bacterial population that was present originally and 3 SRT to wash-out at least 95 %. In this study a mixed culture of '*Candidatus Accumulibacter phosphatis*' and '*Candidatus Competibacter phosphatis*' was obtained after an enrichment period of 14 SRT under phosphate limiting conditions, which comprised 49 ± 6 % '*Candidatus Accumulibacter phosphatis*' clade II and 46 ± 7 % '*Candidatus Competibacter phosphatis*'. Therefore, this

study clearly demonstrated that '*Candidatus Accumulibacter phosphatis*' clade II were able to proliferate under phosphate limiting conditions. In a previous study, the '*Candidatus Accumulibacter phosphatis*' fractions were determined in six activated sludge treatment plants in the Netherlands (Lopez-Vazquez et al. 2008), ranging from 6 to 16 % (with an average of 9.2 %) of the total bacterial community, while the '*Candidatus Competibacter phosphatis*' fractions ranged from 0.4 to 3.2 % (showing an average of 1.7 %). The considerably higher '*Candidatus Accumulibacter phosphatis*' fraction (49 %) obtained in the enriched culture of this study suggests that with practically depleted poly-P reserves '*Candidatus Accumulibacter phosphatis*' clade II were still able to compete with ordinary heterotrophic bacteria by taking up VFA in the anaerobic phase using a metabolism that is not dependent on poly-P. The stoichiometry of the anaerobic carbon and phosphate conversions confirmed that the mixed population made full use of a '*Candidatus Competibacter phosphatis*' metabolism under anaerobic conditions (Table 2). Additional experiments confirmed that under aerobic conditions PAO were able to perform a '*Candidatus Accumulibacter phosphatis*' metabolism when phosphate was added to the system (Fig. 3). These results are in line with previous findings regarding a '*Candidatus Competibacter phosphatis*' enrichment study performed by Lopez-Vazquez et al. (2007), in which a mixed culture was obtained containing 75 % '*Candidatus Competibacter phosphatis*' and 20 % '*Candidatus Accumulibacter phosphatis*' after an enrichment period of 10 SRT. In two previous '*Candidatus Competibacter phosphatis*' enrichment trials performed by the authors of the present study, a reactor was inoculated with sludge from a highly enriched '*Candidatus Accumulibacter phosphatis*' clade II reactor (Welles et al. 2015) assuming that the sludge contained '*Candidatus Competibacter phosphatis*' since most of HAc was taken up through a GAO metabolism. In addition, it was expected that any PAO present would rapidly be washed out of the system due to the low influent P concentration (assuming that they were fully dependent on poly-P) leading to a highly enriched '*Candidatus Competibacter phosphatis*' culture. However, in those enrichment trials FISH analyses revealed that (i) the sludge used as inoculum was rich in '*Candidatus Accumulibacter phosphatis*' II and did not contain '*Candidatus Competibacter phosphatis*' (Welles et al. 2015) and (ii) that under phosphate limiting conditions (like those applied in the present study) '*Candidatus Accumulibacter phosphatis*' II were still dominant after 15 and 16 SRT of operation (data not shown). In spite of the presumably low poly-P contents, those cultures were able to completely remove HAc during the anaerobic phase.

Table 2 Comparison of stoichiometric and kinetic values of the anaerobic conversions determined in this study and previous studies with enriched PAO and GAO cultures

References	Sequencing batch reactor (SBR) Batch reactor (BR),	Organisms PAO II, PAO I, PAO, GAO	SRT (days)	HRT (h)	pH	Influent $[Ca^{2+}]$ (mg l ⁻¹)	VSS/TSS (mg mg ⁻¹)	PHV/PHB (C-mol C-mol ⁻¹)	PHV/HAc (C-mol C-mol ⁻¹)	PHB/HAc (C-mol C-mol ⁻¹)	P/HAc (P-mol C-mol ⁻¹)	Gly/HAc (C-mol C-mol ⁻¹)	q_{SAana}^{MAX} (C-mol h ⁻¹) ⁻¹
This study	SBR	PAO II and GAO	8	12	7 ± 0.1	3.8	0.96	0.37	0.54	1.45	0.03	1.28	0.14
Zeng et al. (2003)	SBR	GAO	6.6	8	7 ± 0.1	6.8	0.97	0.38	0.52	1.39	NA	1.20	0.16–0.18
Lopez-Vazquez et al. (2007)	SBR	GAO	10	12	7 ± 0.1	3.8	0.9	0.34	0.69	1.28	0.01	1.20	0.20
Welles et al. (2015)	SBR	PAO II	8	12	7 ± 0.05	3.8	0.75	0.19	0.23	1.24	0.22	0.96	0.15
	BR	PAO II	NA	NA	7 ± 0.1	3.8	0.93	0.27	0.32	1.19	0.01	0.98	0.08
	SBR	PAO I	8	12	7 ± 0.1	3.8	0.58	0.07	0.09	1.27	0.64	0.29	0.18
	BR	PAO I	NA	NA	7 ± 0.1	3.8	0.95	0.33	0.37	1.09	0.02	1.28	0.02
Zhou et al. (2008)	SBR	PAO	8	24	7.0–8.0	1.3	0.6	0.06	0.07	1.18	0.62	0.46	NA
	BR	PAO	NA	NA	7.5 ± 0.01	1.3	NA	0.37	0.46	1.24	0.06	1.03	0.07
Acevedo et al. (2012)	SBR	PAO I	8	12	7.0–8.9	10	0.45	0.04	0.05	1.31	0.7	0.38	NA
	SBR	PAO I, II	8	12	7.0–8.9	10	0.92	0.16	0.28	1.74	0.08	1.08	NA
Tian et al. (2013)	SBR	PAO I	16	12	7 ± 0.1	3.8	NA	0.1	0.13	1.31	0.56	0.55	NA
Welles et al. 2014	SBR	GAO	8	12	7.0	3.8	0.97	NA	NA	NA	0.012	1.2	0.15
Filipe et al. (2001)	SBR	?	7	12	6.8–7.1	3.8	NA	0.31	0.38	1.26	NA	0.83	0.24
Sudiana et al. (1999) Reactor AL ^a	SBR	?	NA	NA	6.8–7.2	NA	NA	0.24	0.4	1.7	0.02	1.30	0.06–0.08
Liu et al. (1997) ^a	SBR	?	8	6	7 ± 0.1	7.6	NA	NA	NA	NA	0.02	1.37	0.04
Schuler and Jenkins (2003) ^a	SBR	?	4	12	7.15–7.25	16	NA	NA	NA	NA	0.11	1.19	0.03

q_{SAana}^{MAX} specific maximum anaerobic HAC-uptake rate
NA not applicable

^a Calculated assuming that the VSS fully comprised of active biomass

^b DGGE banding patterns indicated that 75 % of the population belonged to γ-proteobacteria, while with FISH analysis, using specific probes developed to target the dominant γ-proteobacteria in the DGGE banding pattern, showed that 35 % of the population stained positive for these γ-proteobacteria

^c FISH analysis revealed that β-proteobacteria were dominant, comprising about one-third of the sludge

Competition between '*Candidatus Accumulibacter phosphatis*' clade I, clade II and '*Candidatus Competibacter phosphatis*'

Enrichment of the specific '*Candidatus Accumulibacter phosphatis*' clade II is in agreement with the findings of Welles et al. (2015a) where clade II showed HAC uptake rates four times higher than those of clade I under poly-P depleted conditions. In those studies, it was suggested that clade II has a competitive advantage over clade I under phosphate limiting conditions. In a study performed by, Tian et al. (2013) an enriched '*Candidatus Accumulibacter phosphatis*' clade I culture was not able to complete the HAC-uptake during the anaerobic phase (36 days SRT, 0.5 days HRT, at 10 °C, pH 7.0 with an influent HAC concentration of 12.5 C-mmol l⁻¹ (375 mg l⁻¹) and an anaerobic phase of 2.25 h) when the phosphate concentration was limiting 0.071 P-mmol l⁻¹ (2.2 mgP l⁻¹ influent ortho-phosphate concentration, resulting in an influent P/C ratio of 0.0056 P-mol C-mol⁻¹). Similar to this observation, Schuler and Jenkins (2003) also observed a leakage of HAC to the aerobic phase (4 days SRT, 0.5 days HRT, 20 °C, pH 7.0, 6.26 C-mmol l⁻¹ (188 mg l⁻¹) influent HAC concentration and 1.83 h anaerobic phase duration) when phosphate became limiting (at an influent P/C ratio lower than 0.019 P-mol C-mol⁻¹). Based on the stoichiometry and kinetic rates reported, it seemed that the culture of Schuler and Jenkins (2003a) was also a '*Candidatus Accumulibacter phosphatis*' clade I dominated culture (Welles et al. 2015). The findings in this study, in the study of Tian et al. (2013) and Schuler and Jenkins (2003a) support the hypothesis that under P-limiting conditions, '*Candidatus Accumulibacter phosphatis*' clade II can proliferate in the system by adjusting its metabolism to low P/C influent ratios while clade I cannot. At high influent P/C ratios (above 0.04 P-mol C-mol⁻¹) with a high poly-P content, clade I may exhibit faster HAC-uptake rates and outcompete clade II.

In the study of Welles et al. (2015) the active biomass specific HAC-uptake rates of PAO (80 C-mmol (C-mol h)⁻¹) determined in short-term batch tests under poly-P depleted conditions seemed to be significantly lower than that of '*Candidatus Competibacter phosphatis*' (150–200 C-mmol (C-mol h)⁻¹) (Zeng et al. 2003; Lopez-Vazquez et al. 2007; Welles et al. 2014), suggesting that '*Candidatus Competibacter phosphatis*' would still be able to outcompete '*Candidatus Accumulibacter phosphatis*' after a few SRT. However, the '*Candidatus Accumulibacter phosphatis*' fractions observed even after enrichment periods of 14–16 SRT were still very significant. This indicates that a population shift from '*Candidatus Accumulibacter phosphatis*' clade II to '*Candidatus Competibacter phosphatis*' needed a long period

due to a high initial '*Candidatus Accumulibacter phosphatis*' clade II/'*Candidatus Competibacter phosphatis*' ratio and a relatively small difference in the HAC-uptake rates of the '*Candidatus Accumulibacter phosphatis*' and '*Candidatus Accumulibacter phosphatis*' enriched in this system. Alternatively, '*Candidatus Competibacter phosphatis*' cultivated under certain controlled operational conditions in laboratory reactors only reach through adaptation their typical maximum activity after a certain period of cultivation and are not directly competitive from the moment of inoculation.

Implications

Limitation of phosphorus has often been used as a strategy to enrich '*Candidatus Competibacter phosphatis*' (Sudiana et al. 1999; Filipe et al. 2001; Zeng et al. 2003; Lopez-Vazquez et al. 2007). This study has demonstrated that it is an unreliable selection strategy that does not always lead to highly enriched '*Candidatus Competibacter phosphatis*' cultures. In addition, the carbon and phosphorus conversions cannot be used as reliable indicators to assess the presence of '*Candidatus Competibacter phosphatis*'. Therefore, to conduct a microbial characterization, using FISH or other microbial identification techniques is always recommended in EBPR studies. Results of previous studies performed on organisms that express the GAO phenotype, without any microbial identification (e.g. Sudiana et al. 1999; Liu et al. 1997; Schuler and Jenkins 2003b), may therefore be questioned, especially if the enrichment period was limited to a few SRT only. The observation that both '*Candidatus Accumulibacter phosphatis*' and '*Candidatus Competibacter phosphatis*' are able to perform a GAO metabolism but at different rates helps to explain the broad range of HAC-uptake rates reported from enriched 'GAO' cultures. In the studies of Sudiana et al. (1999), Liu et al. (1997) and Schuler and Jenkins (2003b) where the presence of '*Candidatus Competibacter phosphatis*' was not reported, HAC-uptake rates range from 0.04 to 0.08 C-mol (C-mol biomass h)⁻¹, while the HAC-uptake rates in studies where the presence of '*Candidatus Competibacter phosphatis*' was confirmed vary between 0.16 and 0.20 C-mol (C-mol biomass h)⁻¹ (Lopez-Vazquez et al. 2007; Zeng et al. 2003; Filipe et al. 2001; Welles et al. 2014). Possibly under P-limited conditions lower HAC uptake rates could be associated to '*Candidatus Accumulibacter phosphatis*' clade II enrichments and higher rates to '*Candidatus Competibacter phosphatis*' enrichments.

This study also suggests that the '*Candidatus Accumulibacter phosphatis*' clade II/'*Candidatus Competibacter phosphatis*' fractions in the inoculum have a significant impact on the time that is needed for enrichment of '*Candidatus Competibacter phosphatis*' cultures

and that a long enrichment period may be needed to obtain highly enriched cultures. Welles et al. (2014) were able to obtain a highly enriched '*Candidatus* Competibacter phosphatis' culture after 44 SRT (352 days) under the same operational conditions, although minor traces of '*Candidatus* Accumulibacter phosphatis' clade II were still present in the biomass. The selection of '*Candidatus* Competibacter phosphatis' may be accelerated when the operating temperature of the reactor is increased (Lopez-Vazquez et al. 2007, 2008), but on the other hand this could lead to selection of specific '*Candidatus* Competibacter phosphatis' that normally prevail in processes at elevated temperature and therefore those '*Candidatus* Competibacter phosphatis' cultures may not be representative in context of the research on wastewater treatment in moderate climate conditions. Further research is needed to define appropriate strategies to enrich '*Candidatus* Accumulibacter phosphatis' clade I, clade II and '*Candidatus* Competibacter phosphatis' for their further study and characterization.

The findings drawn from this study also indicate that temporary limitation of ortho-phosphate by temporal overdosing of iron in activated sludge systems or fluctuations in the influent P/C ratio of industrial wastewater may not have deleterious effects under similar operational conditions (pH = 7.0 and T = 20 °C) on the ability of the activated sludge to perform EBPR once the ortho-phosphate levels in the influent are restored. Past studies have indicated that simultaneous chemical precipitation and enhanced biological phosphorus removal in activated sludge systems, led to a decreased biological phosphorus removal activity and accompanied storage of Poly-P during the periods of iron addition, due to a competition for ortho-phosphate by the chemical and biological mechanisms (De Haas et al. 2000, 2004). However, depletion of poly-P storage pools in '*Candidatus* Accumulibacter phosphatis' clade II, would not severely affect its ability to proliferate in the system and therefore clade II has the potential to remain in the systems for several SRT while performing a GAO metabolism. Once the ortho-phosphate concentrations are restored, '*Candidatus* Accumulibacter phosphatis' clade II may be still present in the system and perform EBPR activity instantly. Temporal overdosing of iron in activated sludge systems or fluctuations in the influent P/C ratio of industrial wastewaters may be problematic in activated sludge systems dominated by '*Candidatus* Accumulibacter phosphatis' clade I but may not be problematic in sludge systems dominated by clade II. Based on the duration of this study and considering that the applied SRT in full-scale activated sludge plants achieving phosphorus and nitrogen removal usually vary between 8 and 30 days, '*Candidatus* Accumulibacter phosphatis' clade II could

be able to prevail in activated sludge systems for 80 up to 300 days under phosphate limiting conditions.

Conclusions

A mixed culture of '*Candidatus* Accumulibacter phosphatis' clade II and '*Candidatus* Competibacter phosphatis' was enriched after a cultivation period of 14–16 SRT under ortho-phosphate limiting conditions. The '*Candidatus* Accumulibacter phosphatis' and '*Candidatus* Competibacter phosphatis' fractions of the total microbial community were around 49 ± 6 and 46 ± 7 %, respectively. In particular, all PAO were closely related to '*Candidatus* Accumulibacter phosphatis' Clade II. Under anaerobic conditions, the mixed culture performed a typical GAO metabolism in which all energy for HAc-uptake was produced by the conversion of glycogen. However, under aerobic conditions '*Candidatus* Accumulibacter phosphatis' were capable of taking up excessive amounts of phosphate when additional phosphate was added to the reactor. This study suggests that limitation of phosphate, often used as a strategy for the enrichment of '*Candidatus* Competibacter phosphatis', does not always lead to high '*Candidatus* Competibacter phosphatis' enrichment and that the carbon conversions often used as indicator for '*Candidatus* Competibacter phosphatis' enrichments are no longer reliable as stand-alone indicators. Furthermore, the development of '*Candidatus* Accumulibacter phosphatis' clade II suggests that clade II has a competitive advantage over clade I under phosphate limiting conditions. From a practical perspective, this study demonstrates that '*Candidatus* Accumulibacter phosphatis' may be able to proliferate under phosphate limiting conditions in activated sludge systems for periods of up to 128 days (16 SRT) or longer while being able to take up phosphate aerobically as soon as it is available in the influent.

Additional file

Additional file 1. FISH-microscopy images used for quantification.

Authors' contributions

All authors contributed to the design of the experiments. LW performed the experiments and drafted the manuscript. All authors read and approved the final manuscript.

Author details

¹ Department of Environmental Engineering and Water Technology, UNESCO-IHE Institute for Water Education, Westvest 7, 2611 AX Delft, The Netherlands.

² Department of Biotechnology, Delft University of Technology, Van der Maasweg 9, 2629 HZ Delft, The Netherlands. ³ KWR watercycle research institute, Groningenhaven 7, Nieuwegein, The Netherlands.

Acknowledgements

This study was carried out as part of the SALINE project (<http://www.saline-sanitation.info>) led by UNESCO-IHE Institute for Water Education with the

consortium partners KWR Watercycle Research Institute, Delft University of Technology, University of Cape Town, The Hong Kong University of Science and Technology, the Higher Polytechnic Institute "José Antonio Echeverría" and Birzeit University.

Competing interests

The authors declare that they have no competing interests.

Received: 4 May 2016 Accepted: 21 June 2016

Published online: 04 July 2016

References

- Acevedo B, Oehmen A, Carvalho G, Seco A, Borras L, Barat R. Metabolic shift of polyphosphate-accumulating organisms with different levels of polyphosphate storage. *Water Res.* 2012;46:1889–900.
- Amann RI, Binder BJ, Olson RJ, Chisholm SW, Devereux R, Stahl DA. Combination of 16S rRNA-targeted oligonucleotide probes with flow cytometry for analyzing mixed microbial populations. *Appl Environ Microbiol.* 1990;56:1919e1925.
- Bond PL, Hugenholtz P, Keller J, Blackall LL. Bacterial community structures of phosphate removing and nonphosphate-removing activated sludges from sequencing batch reactors. *Appl Environ Microbiol.* 1995;61(5):1910–6.
- Bond PL, Erhart R, Wagner M, Keller J, Blackall LL. Identification of some of the major groups of bacteria in efficient and non-efficient biological phosphorus removal activated sludge systems. *Appl Environ Microbiol.* 1999;65(9):4077–84.
- Brdjanovic D, Loosdrecht MCV, Hooijmans CM, Alaerts GJ, Heijnen JJ. Temperature effects on physiology of biological phosphorus removal. *J Environ Eng.* 1997;123(2):144–53.
- Carvalho G, Lemos PC, Oehmen A, Reis MAM. Denitrifying phosphorus removal: linking the process performance with the microbial community structure. *Water Res.* 2007;41(19):4383–96.
- Comeau Y, Hall KJ, Hancock REW, Oldham WK. Biochemical-model for enhanced biological phosphorus removal. *Water Res.* 1986;20(12):1511–21.
- Crocetti GR, Hugenholtz P, Bond PL, Schuler A, Keller J, Jenkins D, Blackall LL. Identification of polyphosphate-accumulating organisms and design of 16S rRNA directed probes for their detection and quantitation. *Appl Environ Microbiol.* 2000;66(3):1175–82.
- Crocetti GR, Banfield JF, Keller J, Bond PL, Blackall LL. Glycogen-accumulating organisms in laboratory-scale and full-scale wastewater treatment processes. *Microbiology.* 2002;148:3353–64.
- Daims H, Bruhl A, Amann R, Amann R, Schleifer KH, Wagner M. The domain-specific probe EUB338 is insufficient for the detection of all bacteria: development and evaluation of a more comprehensive probe set. *Syst Appl Microbiol.* 1999;22:345–52.
- De Haas DW, Wentzel MC, Ekama GA. The use of simultaneous chemical precipitation in modified activated sludge systems exhibiting biological excess phosphate removal. Part 4: experimental periods using ferric chloride. *Water Sa.* 2000;26(4):485–504.
- De Haas DW, Wentzel MC, Ekama GA. The use of simultaneous chemical precipitation in modified activated sludge systems exhibiting biological excess phosphate removal: part 5: experimental periods using a ferrous-ferric chloride blend. *Water Sa.* 2004;27(2):117–34.
- Filipe CDM, Daigger GT, Grady CPL Jr. A metabolic model for acetate uptake under anaerobic conditions by glycogen-accumulating organisms: stoichiometry, kinetics and effect of pH. *Biotechnol Bioeng.* 2001;76(1):17–31.
- Flowers JJ, He S, Yilmaz S, Noguera DR, McMahon KD. Denitrification capabilities of two biological phosphorus removal sludges dominated by different '*Candidatus Accumulibacter*' clades. *Environ Microbiol.* 2009;1(6):583–8.
- Gu AZ, Saunders AM, Neethling JB, Stensel HD, Blackall L. In: WEF, editor. Investigation of PAO and GAO and their effects on EBPR performance at full-scale wastewater treatment plants in US, October 29–November 2. WEFTEC, Washington; 2005.
- He S, Gu AZ, McMahon KD. The role of Rhodocyclus-like organisms in biological phosphorus removal: factors influencing population structure and activity. In: Water environment federation technical exhibition and conference (WEFTEC) 2005, October 29–November 2. Washington; 2005.
- Hesselmann RPX, Werlen C, Hahn D, van der Meer JR, Zehnder AJB. Enrichment, phylogenetic analysis and detection of a bacterium that performs enhanced biological phosphate removal in activated sludge. *Syst Appl Microbiol.* 1999;22(3):454–65.
- Kong YH, Nielsen JL, Nielsen PH. Microautoradiographic study of Rhodocyclus-related polyphosphate-accumulating bacteria in full-scale enhanced biological phosphorus removal plants. *Appl Environ Microbiol.* 2004;70(9):5383–90.
- Lanham AB, Ricardo AR, Coma M, Fradinho J, Carvalho M, Oehmen A, Carvalho G, Reis MA. Optimisation of glycogen quantification in mixed microbial cultures. *Biores Technol.* 2012;118:518–25.
- Liu WT, Nakamura K, Matsuo T, Mino T. Internal energy-based competition between polyphosphate- and glycogen-accumulating bacteria in biological phosphorus removal reactors-effect of P/C feeding ratio. *Water Res.* 1997;31(6):1430–8.
- Lopez-Vazquez CM, Song YI, Hooijmans CM, Brdjanovic D, Moussa MS, Gijzen HJ, Van Loosdrecht MCM. Short-term temperature effects on the anaerobic metabolism of glycogen accumulating organisms. *Biotechnol Bioeng.* 2007;97(3):483–95.
- Lopez-Vazquez CM, Hooijmans CM, Brdjanovic D, Gijzen HJ, Van Loosdrecht MCM. Factors affecting the microbial populations at full-scale enhanced biological phosphorus removal (EBPR) wastewater treatment plants in The Netherlands. *Water Res.* 2008a;42(10):2349–60.
- Lopez-Vazquez CM, Song YI, Hooijmans CM, Brdjanovic D, Moussa MS, Gijzen HJ, van Loosdrecht MCM. Temperature effects on the aerobic metabolism of glycogen accumulating organisms. *Biotech Bioeng.* 2008b;101(2):295–306.
- Metcalfe and Eddy, Inc. Wastewater engineering—treatment and reuse. 4th ed. New York: Mc Graw Hill; 2003.
- Mino T, Arun V, Tsuzuki Y, Matsuo T. Effect of phosphorus accumulation on acetate metabolism in the biological phosphorus removal process. In: Ramadori R, editor. Biological phosphate removal from wastewaters, advances in water pollution control, vol. 4. Oxford: Pergamon Press; 1987. p. 27–38.
- Nielsen AT, Liu WT, Filipe C, Grady L, Molin S, Stahl DA. Identification of a novel group of bacteria in sludge from a deteriorated biological phosphorus removal reactor. *Appl Environ Microbiol.* 1999;65(3):1251–8.
- Oehmen A, Lemos PC, Carvalho G, Yuan Z, Keller J, Blackall LL, Reis MAM. Advances in enhanced biological phosphorus removal: from micro to macro scale. *Water Res.* 2007;41(11):2271–300.
- Schuler AJ, Jenkins D. Enhanced biological phosphorus removal from wastewater by biomass with different phosphorus contents, part 1: experimental results and comparison with metabolic models. *Water Environ Res.* 2003a;75(6):485–98.
- Schuler AJ, Jenkins D. Enhanced biological phosphorus removal from wastewater by biomass with different phosphorus contents, part 2: anaerobic adenosine triphosphate utilization and acetate uptake rates. *Water Environ Res.* 2003b;75(6):499–511.
- Schuler AJ, Jenkins D. Enhanced biological phosphorus removal from wastewater by biomass with different phosphorus contents, part 1: experimental results and comparison with metabolic models. *Water Environ Res.* 2003c;75(6):485–98.
- Slater FR, Johnson CR, Blackall LL, Beiko RG, Bond PL. Monitoring associations between clade-level variation, overall community structure and ecosystem function in enhanced biological phosphorus removal (EBPR) systems using terminal-restriction fragment length polymorphism (T-RFLP). *Water Res.* 2010;44(17):4908–23.
- Smolders GJF, Van der Meij J, Van Loosdrecht MCM, Heijnen JJ. Model of the anaerobic metabolism of the biological phosphorus removal process: stoichiometry and pH influence. *Biotechnol Bioeng.* 1994;43(6):461–70.
- Sudiana IM, Mino T, Satoh H, Nakamura K, Matsuo T. Metabolism of enhanced biological phosphorus removal and non-enhanced biological phosphorus removal sludge with acetate and glucose as carbon source. *Wat Sci Technol.* 1999;39(6):29–35.

- Tian WD, Lopez-Vazquez CM, Li WG, Brdjanovic D, van Loosdrecht MCM. Occurrence of PAOI in a low temperature EBPR system. *Chemosphere*. 2013;92:1314–20.
- Welles L, Lopez-Vazquez CM, Hooijmans CM, Van Loosdrecht MCM, Brdjanovic D. Impact of salinity on the anaerobic metabolism of phosphate—accumulating organisms (PAO) and glycogen—accumulating organisms (GAO). *Appl Microbiol Biotechnol*. 2014;98(12):7609–22.
- Welles L, Tian WD, Saad S, Abbas B, Lopez-Vazquez CM, Hooijmans CM, van Loosdrecht MCM, Brdjanovic D. Accumulibacter clades type I and II performing kinetically different glycogen-accumulating organisms metabolisms for anaerobic substrate uptake. *Water Res*. 2015a;83:354–66.
- Welles L, Lopez-Vazquez CM, Hooijmans CM, van Loosdrecht MCM, Brdjanovic D. Impact of salinity on the aerobic metabolism of phosphate-accumulating organisms. *Appl Microbiol Biotechnol*. 2015b;99(8):3659–72.
- Wentzel MC, Dold PL, Ekama GA, Marais GvR. Kinetics of biological phosphorus release. *Water Sci Technol*. 1985;17:57–71.
- Wong MT, Mino T, Seviour RJ, Onuki M, Liu WT. In situ identification and characterization of the microbial community structure of full-scale enhanced biological phosphorous removal plants in Japan. *Water Res*. 2005;39(13):2901–14.
- Zeng RJ, van Loosdrecht MCM, Yuan Z, Keller J. Metabolic model for glycogen-accumulating organisms in anaerobic/aerobic activated sludge systems. *Biotechnol Bioeng*. 2003;81(1):92–105.
- Zhou Y, Pijuan M, Zeng RJ, Lu H, Yuan Z. Could polyphosphate-accumulating organisms (PAO) be glycogen-accumulating organisms (GAO)? *Water Res*. 2008;42:2361–8.
- Zilles JL, Peccia J, Kim MW, Hung CH, Noguera DR. Involvement of Rhodocyclus-related organisms in phosphorus removal in full-scale wastewater treatment plants. *Appl Environ Microbiol*. 2002;68(6):2763–9.

Submit your manuscript to a SpringerOpen[®] journal and benefit from:

- Convenient online submission
- Rigorous peer review
- Immediate publication on acceptance
- Open access: articles freely available online
- High visibility within the field
- Retaining the copyright to your article

Submit your next manuscript at ► springeropen.com
